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**Second Semester M.Tech. Degree Examination, June/July 2014**  
**Advanced Heat Transfer**

Time: 3 hrs.

Max. Marks: 100

**Note: 1. Answer any FIVE full questions.****2. Use of heat transfer and thermodynamics data hand book is permitted.**

- 1
  - a. Briefly discuss on different modes of heat transfer and state the fundamental laws governing them. (06 Marks)
  - b. Starting from fundamentals derive the differential equation for temperature distribution in a fin. (08 Marks)
  - c. In conductivity measuring experiment two identical long rods are used. One rod is made of aluminium ( $k = 200 \text{ W/mk}$ ), while the other rod is a specimen. One end of both rods are fixed to a wall at  $100^\circ\text{C}$ , while the other end is suspended in air at  $25^\circ\text{C}$ . The steady temperature at same distance along the rods were measured and found to be  $75^\circ\text{C}$  on a aluminium rod and  $60^\circ\text{C}$  on specimen rod. Find thermal conductivity  $K$  for specimen assuming insulated tip. (06 Marks)
  
- 2
  - a. Define conduction shape factor and explain its significance. (06 Marks)
  - b. Two parallel 50cm diameter disks are separated by a distance of 1.5m in an infinite medium having  $K = 2.3 \text{ W/m}^\circ\text{C}$ . One disk is maintained at  $80^\circ\text{C}$  and the other at  $20^\circ\text{C}$ . Calculate the conduction shape factor and the heat transfer between the disks. (08 Marks)
  - c. Explain the method of solving a 2-d heat conduction problem using electrical analogy. (06 Marks)
  
- 3
  - a. State the following laws as applied to thermal radiation:
    - i) Kirchoff's law
    - ii) Stefan-Boltzmann law
    - iii) Wien's displacement law
    - iv) Lambert's cosine law. (08 Marks)
  - b. Two very large planes with emissivities 0.3 and 0.8 exchange heat. Find the percentage reduction in heat transfer when a polished-aluminum radiation shield ( $\epsilon = 0.04$ ) is placed between them. (12 Marks)
  
- 4
  - a. Derive the momentum equation for the laminar boundary layer on a flat plate. State the assumptions made. (10 Marks)
  - b. Air at  $20^\circ\text{C}$  and atmospheric pressure is flowing over a flat plate at a velocity of 3 m/s. If the plate is 30cm wide and at a temperature of  $60^\circ\text{C}$ . Calculate the following quantities at  $x = 0.3\text{m}$ :
    - i) Thickness of velocity and thermal boundary layer.
    - ii) Local and average friction coefficient.
    - iii) Local and average heat transfer coefficient.
    - iv) Total drag force on the plate.

At 313K take the following properties of air  $\rho = 1.18\text{kg/m}^3$ ;  $\gamma = 17 \times 10^{-6}\text{m}^2/\text{s}$ ;  
 $k = 0.0272 \text{ W/m}^\circ\text{C}$ .  $C_p = 1.007 \text{ kJ/kg}^\circ\text{C}$ ,  $P_r = 0.705$ . (10 Marks)

- 5 a. Derive an expression for forced convection heat transfer in terms of dimensionless parameters using dimensional analysis. (10 Marks)
- b. Air at 2 atm and 200°C is heated as it flows through a tube with a diameter of 25.4mm at a velocity of 10m/s. Calculate the heat transfer per unit length of the tube if a constant heat flux condition is maintained at the wall and the tube wall temperature is 20°C above the air temperature, all along the tube length. How much would the bulk temperature increase over a 3m length of the tube? Take properties of air at a bulk temperature of 200°C as,  $\rho = 1.493 \text{ kg/m}^3$ ;  $P_r = 0.681$ ;  $\mu = 2.57 \times 10^{-5} \text{ kg/m-s}$ ;  $k = 0.0386 \text{ W/m}^\circ\text{C}$ ;  $C_p = 1.025 \text{ kJ/kg}^\circ\text{C}$ . (10 Marks)
- 6 a. Define and explain the significance of
- Reynolds number
  - Prandtl number
  - Grashof number
  - Nusselt number.
- (08 Marks)
- b. A hot square plate 50cm  $\times$  50cm at 100°C is exposed to atmospheric air at 20°C. Find the heat loss from both surfaces of the plate if i) Plate is kept vertical; ii) Plate is kept horizontal. Use the following relation:  
 $Nu = 0.13 (GrPr)^{1/3}$  for vertical position.  
 $Nu = 0.71 (GrPr)^{1/4}$  for upper surface.  
 $Nu = 0.35 (GrPr)^{1/4}$  for lower surface. (12 Marks)
- 7 a. Derive an expression for effectiveness of a counter flow heat exchanger in terms of number of transfer units (N) and heat capacity ratio of two fluids (C). (10 Marks)
- b. Find out the length of tube required for the following heat transfer in a parallel flow heat exchanger where air is heated by exhaust gases  $Q = 9.3 \text{ kW}$ ,  $d_i = 5\text{cm}$ ,  $d_o = 6\text{cm}$ ,  $h_i = 116 \text{ W/m}^2^\circ\text{C}$ ,  $h_o = 186 \text{ W/m}^2^\circ\text{C}$ . Inlet and outlet temperatures of hot fluid are respectively 400°C and 150°C, and for cold fluid are respectively 50°C and 100°C. Neglect tube resistance. If the flow is made counter flow, what is the percentage of saving in tube length? (10 Marks)
- 8 a. Explain the different regimes of pool boiling using an appropriate boiling curve. Indicate CHF and Leiden Frost points on it. (10 Marks)
- b. Air free saturated steam at 85°C and pressure of 57.8 kPa condenses on the outer surface of 225 horizontal tubes of 1.27 cm OD arranged in a square array. The surface is maintained at a uniform temperature of 75°C. Calculate the total condensation rate per meter length of the tube bundle. (10 Marks)

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